

**AMENDMENTS TO THE SPECIFICATION**

Please insert the reference number "3A" after the word "end" on page 9, line 2. The paragraph beginning on page 8, line 23 and ending on page 9, line 2 will thereby be amended to read as follows:

In the method for producing low-temperature coke without further solids, which is shown in FIG. 1, fine-grained coal with a grain size of less than 10 mm is charged into the low-temperature carbonization reactor 2 via conduit 1. In its lower central region, the reactor 2 has a vertical central tube 3 which is surrounded by a chamber 4 which is annularly formed in cross-section. The chamber 4 is divided into an upper part and a lower part by a gas distributor 5. While the lower chamber acts as gas distributor chamber for fluidizing gas, a stationary fluidized bed 6 (annular fluidized bed) of fluidized coal is located in the upper part of the chamber, the fluidized bed extending a bit beyond the upper orifice end 3A of the central tube 3

Please insert the reference number "3A" after the word "region" on page 9, line 19. The paragraph beginning on page 9, line 12 and ending on page 10, line 4 will thereby be amended to read as follows:

Through the central tube 3 air is likewise constantly supplied to the low-temperature carbonization reactor 2, which air upon passing through the central tube 3 flows through the mixing chamber region 8 and the upper duct 9 into the cyclone 10. The velocity of the gas supplied to the reactor 2 preferably is adjusted such that the Particle-Froude-Number in the central tube 3 is between 6 and 10. Due to the high velocity, the air flowing through the central tube 3 entrains solids from the stationary annular fluidized bed 6 into the mixing chamber region 8 upon passing through the upper orifice region 3A, so that an intensively mixed suspension is formed. As a result of the reduction of the flow velocity by the

expansion of the gas jet and/or by impingement on one of the reactor walls, the entrained solids quickly lose velocity and fall back into the annular fluidized bed 6. Only a small amount of non-precipitated solids is discharged from the low-temperature carbonization reactor 2 together with the gas stream via the duct 9. Thus, between the reactor regions of the stationary annular fluidized bed 6 and the mixing chamber 8 a solids circulation is obtained, by means of which a good mass and heat transfer is ensured. The solids retention time in the reactor can be adjusted within wide limits by the selection of height and outside diameter of the annular fluidized bed 6. Solids separated in the cyclone 10 are fed into the product discharge conduit 12 via conduit 11, whereas the still hot exhaust gas is supplied via conduit 13 into another cyclone 14, separated there from possibly remaining solids, and withdrawn via an exhaust gas conduit 15. Solids separated in the cyclone 14 are supplied again to the reactor 2 via conduit 16 for low-temperature carbonization.

Please insert the following paragraph after the paragraph stating "3 gas supply tube (central tube)" on page 14, line 5:

"3A upper orifice end/region"